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# Implementation of a Simplified Micromixing Model Inside a Lagrangian Particle Dispersion Code for the Estimation of Concentration Variances and Peaks

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In the frame of the modelling simulation of odour nuisances, the estimation of concentration peaks, representing values averaged over a relatively short time of the order of the interval between subsequent breathes, is of fundamental importance. Dispersion models currently used in this field cannot reconstruct this kind of values at relatively high frequency, due to their intrinsic theoretical design that allows to give time- or ensemble average-concentrations only. The scope of this work is to describe the implementation of a simplified micromixing model inside a standard ensemble average Lagrangian Particle Dispersion Model, with the aim of simulating the field of concentration variances together with concentration averages. A simplified micromixing model represents a way to describe the interaction between the part of the emitted plume and the rest of the atmospheric flow, derived through bulk entrainment relationships. This simplified view allows the description of the first two moments of the concentration distribution which is however sufficient to describe a peak-to-mean relationship making some hypotheses about the form of the distribution. Some preliminary results of the application of this method inside the SPRAY Lagrangian Particle Dispersion Model are shown, comparing both the instantaneous concentration and the peak-to-mean ratio together with their spatial behaviour derived in some controlled conditions with those obtained from the application of other schemes currently included in the code.

## 1. Introduction

Atmospheric dispersion models are widely used tools to give a spatial and temporal description of the concentrations of emitted substances that could potentially generate different problems to the population. In most of their applications, typically related to the comparison with air quality regulatory rules, atmospheric dispersion models are used to reconstruct mean concentrations representing for example the average over time intervals of the order of 1 hour. There exist some specific applications, as the dispersion of explosive or flammable, toxic or odorous emissions, where the simple reconstruction of the mean value is not sufficient due to the intrinsic characteristics of the consequences generated by the involved substances. In particular, the sensation of olfactory nuisance occurs in an individual during the normal respiratory activity happening at a relatively high frequency, typically every less than 10 seconds. This implies that the reconstruction of the impact generated by the odorous emissions should in principle take into account this peculiarity and a reconstruction of the short-term concentrations, which are more assimilated to instantaneous events, is potentially required (Capelli et al., 2013). This means that models should include a way to predict also concentration fluctuations or a statistical indicator to describe them. The availability of both the average concentrations and concentration fluctuations as model output, allows to make a more complete and correct estimation of the impact that odorous emissions can have on the population. Not many of the typical models used in the framework of odour impact have a direct mechanism inside to fulfil this request. A useful review of the efforts made by the scientific community in the last seventy years to include the reconstruction of concentration fluctuations inside dispersion models can be found in Cassiani et al. (2020). A particular attention was devoted to Lagrangian one-particle dispersion models, derived from the fundamental work of Thomson (1987), and widely used in the frame of air quality to reconstruct ensemble average concentrations over complex terrain. Different methods have been

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## 2. Theoretical description of the SPRAY model

In the Lagrangian Particle SPRAY code, the dispersion of an airborne pollutant is simulated following the motion of a large number of fictitious particles. Each particle moves through a "transport" component of the velocity provided by an external meteorological driver and a stochastic or "turbulent" component obtained by solving a 3-D form of a Langevin equation defined in its general form, following Thomson (1987) as:

$$du_i = a_i(\mathbf{x}, \mathbf{u}, t)dt + b_{ii}(\mathbf{x}, \mathbf{u}, t)dW_i(t)$$

where **x** represents the vector of the particle position, and **u** the Lagrangian velocity vector,  $a_i(x, u, t)dt$  is a deterministic term depending on Eulerian probability density function (PDF) of the turbulent velocity, determined from the Fokker–Planck equation and  $b_{ij}(x, u, t)dW_j(t)$  represents a stochastic term where  $dW_j(t)$  is the incremental Wiener process. Each particle carries a mass of pollutants that in case of odorous emission can be considered in terms of "Odour Units" and ensemble average concentrations can be computed considering the total mass of all the particles contained into control volumes of a 3D grid. Although Lagrangian Particle Dispersion Models are used in many situations to describe the dispersion in complex conditions, they cannot in principle directly address the calculation of concentration fluctuations useful for a correct estimation of instantaneous concentrations.

Currently, the simplified VTE method to compute concentration variances is implemented into the SPRAY code as follows. An instantaneous concentration c can be supposed as the sum of an (time or ensemble) average value C plus a fluctuation c'. In general, the conservation equation for the concentration variance  $c^2$  can be written (Stull, 1989, Milliez and Carissimo, 2008) in the following form:

$$\frac{\partial \overline{c'^2}}{\partial t} + U_j \frac{\partial \overline{c'^2}}{\partial x_j} = -2\nu_C \overline{\left(\frac{\partial c'}{\partial x_j}\right)^2} - \frac{\partial}{\partial x_j} (\overline{u_j'c'^2}) - 2\overline{u_j'c'} \left(\frac{\partial C}{\partial x_j}\right)^2$$

where the two terms on the left represent the storage and advection, the first term on the right represents the viscous dissipation, the second one represents the divergence of the turbulent flow and the third one the source term for the variance, proportional to the average concentration gradient. Following Hsieh (2007) and Milliez and Carissimo (2008) an algebraic closure for the molecular dissipation can be rewritten as:

$$-2\nu_{c}\left(\frac{\partial c'}{\partial x_{j}}\right)^{2} = \varepsilon_{c} = \frac{\overline{c'^{2}}}{t_{d}}$$

where *t<sub>d</sub>* represents a dissipation time scale characteristic of the concentration variance decay. For the third order term representing the turbulent divergence of the concentration variance a K closure can be adopted, obtaining:

$$\overline{u'_j c'} = -K_j \frac{\partial c}{\partial x_j} \qquad \text{where:}$$
  

$$K_j = \sigma_{u_j}^2 T_{L_j}$$

Oettl and Ferrero (2017) evaluated the relative importance of the various terms inside the conservation equation for the concentration variance through some considerations derived from available measurements. As a result, they estimated that the advection term on the left and the diffusion term on the right can be reasonably neglected, obtaining an equation independent from the mean flow field in the form:

$$\frac{\partial \overline{c'^2}}{\partial t} = 2\sigma_{u_j}^2 T_{L_j} \left(\frac{\partial C}{\partial x_j}\right)^2 - \frac{\overline{c'^2}}{t_d}$$

This equation has the following analytical solution:

$$\overline{c'^2} = 2\sigma_{u_j}^2 T_{L_j} t_d \left(\frac{\partial C}{\partial x_j}\right)^2 \left[1 - e^{(-t/t_d)}\right]$$

It is suggested (Ferrero et al., 2020) that the approximation represented by the last relationship can be considered acceptable for the calculation of the concentration variance, once the turbulent variables and the average concentration field are known. Using the average concentration field directly computed by the code and the turbulent variables considered for the particle movement, a time varying concentration variance field is calculated with the previous relationship on the same grid considered for the average concentrations. It is supposed that  $t_d = T_{Lw}$ . Once the concentration variance is computed, the peak concentration is then estimated considering the 98 percentile of a two parameters Weibull distribution having the known average concentration and concentration variance.

#### 2.1 Simplified Micromixing VPA model

A micromixing model (or PDF model) simulates the intrinsically continuous Planetary Boundary Layer as a geometric space in which a very large number of air particles, each fully detectable, are uniformly distributed. Each of them is completely characterized at a generic instant *t* by:

- a position in space **X**(t),
- a velocity fluctuation **u**(**X**,t) with respect to a mean (Eulerian) field of motion **U**(X,t),
- a concentration of the interested pollutant C(X,t).

At each instant *t* prior to an initial instant *t*<sub>0</sub> all particles (initially uniformly distributed in space) possess a concentration  $C(t < t_0) = 0$ . At a given initial time *t*<sub>0</sub>, some of these particles will transit through the source (e.g. a point source) and will acquire mass from it and therefore an initial concentration  $C_0(t_0)$ , while all the others will continue to keep zero concentration. From the instant *t*<sub>0</sub> onwards, the model will begin to simulate the dispersion of all the particles (both those with non-zero concentration and those with zero concentration), considering their different stochastic trajectories and their mutual interaction. This interaction is constituted by a mass exchange of the pollutant between a generic particle and the adjacent particles, induced by molecular diffusivity and driven by the turbulence that characterizes locally the PBL. Therefore, the model will simulate the trajectory of all particles as a normal Lagrangian one-particle model with the additional practical problem related to the huge number of particles whose trajectory and mass exchange must be simulated.

In a micromixing model, the pollutant exchange among close particles is modelled, for simplicity, through a bulk law describing, for each particle, the mass exchange with the adjacent external environment, simulated as a continuous fluid characterized by an average concentration C. In practice, for the *p*-th particle this exchange is described by the following micromixing relation that simulates the action of molecular diffusivity:

$$\frac{dC^{p}(\boldsymbol{X}_{p},t)}{dt} = -\frac{C^{p}(\boldsymbol{X}_{p},t) - \overline{C(\boldsymbol{X}_{p},t)}}{\tau_{m}}$$
(1)

where  $\tau_m$  represents the so-called micromixing time scale. Some particles will decrease in concentration (those passing through the source) while others (those that constitute the surrounding air) will increase it.

Assuming to divide the entire computational domain in cells, at the end of the time step there will be  $N_k$  particles in the *k*-th cell, each with its own concentration. The average characteristic concentration of the cell can be computed as:

$$\overline{C_k}(t) = \frac{1}{N_k} \sum_{p=1}^{N_k} C^p(t)$$

while the second moment can be computed as:

$$\overline{C_k^2}(t) = \frac{1}{N_k} \sum_{p_{-1}}^{N_k} \left( C^p(t) \right)^2$$

and the concentration variance can be computed as:

$$(\sigma_c^2)_k = \overline{\mathcal{C}_k^2}(t) - \left(\overline{\mathcal{C}_k}(t)\right)^2 \tag{2}$$

To overcome the problem of simulating a huge number of particles, both those emitted by the considered sources and those referring to the background, Cassiani (2013) proposed the VPA approach. This approach, allows to consider only the particles emitted by the source, as during the normal execution of the SPRAY code. To this aim, the volume  $V_p$  is added to each particle as an additional property. Considering the appropriate initial conditions for the particle volume, related mainly to the initial source size, it is possible to define the evolution of the particle concentration from its initial value, as described in equation (1), during a model discretization time step. Since the particle mass must be conserved, this means that also a change in volume must be considered as:

$$V^{p}(t + \Delta t) = V^{p}(t) \left( \frac{C^{p}(t)}{C^{p}(t) + \Delta C^{p}} \right)$$

In the current implementation of the VPA model inside SPRAY, the micromixing time scale  $\tau_m$  is defined, as described in Dixon and Tomlin (2007), with the following simplified formula:

 $\tau_m = 0.75 \, k/\varepsilon$ 

where k represents the turbulent kinetic energy and  $\mathcal{E}$  represents its dissipation rate. Both terms can be calculated in each point using the variables that define the turbulence parameters inside the code. Once the average concentrations are computed and concentration variances are estimated using (2), then the peak concentration is calculated as the 98 percentile of a two parameters Weibull distribution.

#### 3. Results

## 3.1 Peak-to-mean in controlled conditions

To obtain some preliminary results, a simulation in controlled conditions has been performed in order to compare the results between the VTE and VPA methods. A 12 x 12 km<sup>2</sup> computational domain with flat terrain and a surface roughness of 0.1 m has been considered. The meteorological conditions consider a constant mean wind of 1 m/s blowing towards North and unstable convective stability conditions characterized by a Monin-Obuhkov length of -10 m, a vertical mixed layer of 1500 m and a convective velocity scale of 0.2 m/s. In these conditions, a neutrally buoyant point source with stack height = 10 m, stack diameter = 0.5 m, stationary emitting flow = 1700 eu/s has been simulated, where eu represents generic "emission units" that can be interpreted as odour units in case of odour emissions or mass units in case of pollutant mass emissions. Figure 1a represents the average concentration field close to the ground given by the standard dispersion model, while Figure 1b and Figure 1c reproduce peak concentrations using the VTE method and the VPA method respectively, as described in Chapter 2. For both methods, peak concentration fields show a pattern evidently larger than the one of average values, with values systematically higher in each simulated point. The VTE method shows larger concentration values in the proximity to the source with a maximum of 5 eu/m<sup>3</sup>, compared to a maximum of the average value at the same point of 1.57 eu/m3 (corresponding to a peak-to-mean value for the maximum average concentration of 3.18). The VPA method shows instead a larger pattern extending to a greater distance from the source, even if characterized by smaller concentrations close to the emission with a maximum of 1.96 eu/m<sup>3</sup> (corresponding to a peak-to mean value for the maximum average concentrations of 1.25 only).



Figure 1: ground level average concentrations (a), peak concentrations using VTE method (b) and peak concentrations using VPA method (c)

To have a clearer view of the spatial behaviour of the peak values and their relationship with the average concentrations, two sections along the x axis of the ground level average and peak concentrations have been

extracted corresponding to the two horizontal dashed and continuous lines depicted in Figure 1 a,b,c, located 1 and 5 km downwind the source respectively. Figures 2a and 2b illustrate the behaviour of average and peak concentrations at the 1 km and 5 km horizontal sections respectively. Along section 1, closer to the source, VPA method shows similar values with respect to VTE with slightly larger values close to the plume centreline where a peak-to-mean ratio is about to 1.75 for VPA and 1.55 for VTE. Moving away from the source position, the VPA method shows a clearer signal, with larger peak values compared to VTE methods and a peak-to-mean ratio close to the plume centreline of about 2.4 for VPA and 1.54 for VTE.



Figure 2: ground level average and peak concentrations at the two sections along x axis 1 km (a) and 5 km (b) downwind the source position.

A preliminary comparison of the peak-to-mean ratios obtained by the VPA model against crosswind theoretical values 250 m downwind the source position obtained by a semi-empirical Gaussian Plume model validated with experiments by Léfstrom at al. (1994) in unstable conditions is illustrated in Figure 3, showing promising results.



Figure 3: comparison of crosswind peak-to-mean ratios 250 m downwind source in unstable conditions obtained by the semi-empirical Gaussian model validated in Lofstrom et al. (1994) and results from the VPA model

#### 3.2 Comparison with constant peak-to-mean ratio

It is a common procedure, in the frame of odour applications, to calculate peak concentrations by applying a simple peak-to-mean ratio, kept uniformly constant throughout the domain and over time. This way of operating is meant to represent a sort of precautional procedure, giving safe peak values everywhere. As an example, although there is not a legislation at national level, some Italian guidelines are applied at a regional level, suggesting the use of a constant 2.3 peak-to-mean ratio. It is hence interesting to understand the differences that can arise using the two VTE and VPA methods introduced here and a simplified procedure in the calculation of peak concentrations. Figures 4a and 4b illustrate the absolute differences between peak values computed using VTE and VPA methods respectively and those computed applying a 2.3 uniform peak-to-mean ratio. In the figure, regions represented by colours from green to red are those containing a peak-to-mean ratio larger than 2.3, while regions in blue are those with peak-to-mean smaller. Both VTE and VPA methods calculate a non-uniform distribution of the peak-to-mean ratio both with a general similar behaviour showing smaller than 2.3 values downwind the source close to the plume centreline and larger than 2.3 values close to the plume external border. The VTE method gives larger peak concentrations close to the source, where the VPA method doesn't calculate such big values. The VPA method shows instead peak-to-mean ratios significantly higher than the constant 2.3 factor also at large distances from the source, where the VTE method doesn't manifest such big values.



Figure 4: absolute differences between peak concentrations at ground computed using the VTE method (a) and VPA method (b) and the application of a 2.3 constant peak-to-mean ratio.

## 4. Conclusions

A simplified micromixing model (VPA) was introduced inside the Lagrangian Particle Dispersion Model SPRAY with the aim of calculating concentration variances and estimating peak concentrations, specifically required to reconstruct the impact of odorous emissions. This method allows to take into consideration only the particles related to the emissions, increasing the computational efficiency with respect to a standard micromixing method that requires to follow also particles representing the atmospheric background. The micromixing model has been compared in a controlled condition with another existing method already present in the code implementing a simplified form for the transport equation of the concentration variance (VTE). Both methods show a general behaviour of giving non uniform peak-to-mean ratios with larger peak concentrations close to the plume border and smaller around the plume centreline. Results show that the VTE method determines higher peaks close to the source, with peak-to-mean ratios that can be significantly larger than a factor 3, while the VPA method shows smaller peak-to-mean ratios close to the source but extending over regions further away from the source, even for more than 5 km. These preliminary results must be confirmed through a comparison with available measured data in a real environment and this validation procedure will be implemented in the next future.

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