

Data analysis and inference for an industrial deethanizer

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In this paper, we present an application of data derived approaches for analyzing and monitoring an industrial deethanizer column. The discussed methods are used in visualizing process measurements, extracting operational information and designing an estimation model. Emphasis is given to the modeling of the data obtained with standard paradigms like the Self-Organizing Map (SOM) and the Multi-Layer Perceptron (MLP). Here, the effectiveness of these data-derived techniques is validated on a full-scale application where the goal is to identify significant operational modes and most sensitive process variables before developing an alternative control scheme.

1. Introduction

A modern process plant is under tremendous pressure to maintaining and improving product quality and profit under stringent environmental and safety constraints. For efficient operation, any decision-making action related to the plant operation requires the knowledge of the actual state of the process. The availability of easily accessible displays and intuitive knowledge of the states is invaluable with immediate implications for profitability, management planning, environmental responsibility and safety.

In this paper, we discuss the implementation and direct application of a strategy to model, visualize and analyze the information encoded in industrial process data. The approach is based on a classical machine learning method for dimensionality reduction and quantization, the Self-Organizing Map, SOM (Kohonen 2001). The SOM combines many of the main properties of other general techniques and shares many commonalities with two standard methods for data projection (Principal Components Analysis) and clustering (K-means). In addition, the SOM is also provided with a set of tools that allow for efficient data visualizations in high-dimensional settings. The use of the Self-Organizing Map in the exploratory stage of data analysis is discussed in (Kaski, 1997 and Vesanto, 2002) and it is widely employed in many fields.

2. The Self-Organizing Map

The Self-Organizing Map is an adaptive neural paradigm to performing in unison:

- A reduction of the data dimensionality by projection; that is, the reduction of the dimensionality of the data by mapping all the observations onto meaningful subspaces with lower dimensionality.
- A reduction of the amount of data by clustering; that is, the retention of the original dimensionality of the data space while reducing the amount of observations by grouping them according to similarity.

The SOM nonlinearly projects vast quantities of high-dimensional data onto a lower-dimensional array of fewer prototypes in a fashion that aims at preserving the topology of the observations. By choosing a bi-dimensional array of prototypes, the SOM is to be understood as an ordered image of the original high-dimensional data manifold as modeled onto a low-dimensional subspace where the complex data structures are represented by simple geometric relationships. In this case, the SOM offers excellent techniques for data exploration. The SOM algorithm is described by Kohonen (2001).

The data visualization techniques based on the SOM assume that the prototype vectors are representative models for similar groups of observations, and projecting the data onto the low-dimensional array allows for an efficient display of the dominant relationships existing between them. The visualization techniques considered here are i) the component planes and ii) the distance matrix (Kaski, 1997 and Vesanto, 2002).

3. Case study

To illustrate the potentialities of topological data analysis using the Self-Organizing Map, the overviewed methods are applied to a monitoring problem consisting of modeling and analyzing the operational behavior of an industrial deethanizer, starting from a set of online process measurements. The objective of the deethanizer, in Fig. 1, is to separate ethane from the feed stream (a light naphtha) while minimizing the ethane extracted from the bottom of the column (an economical constraint for the subsequent unit in the plant). Such a constraint is quantified by the maximum amount of ethane lost from the column bottom; the operational threshold is set be smaller than 2%.

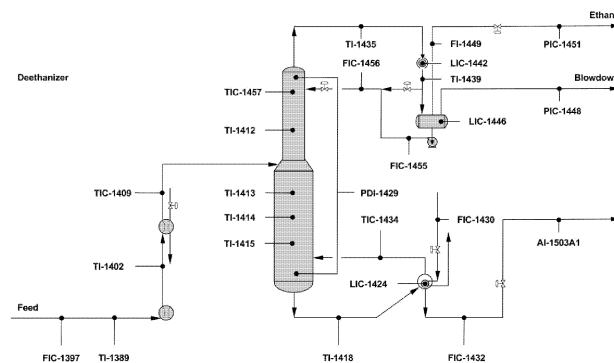


Figure 1 Deethanizer: Simplified flow-sheet.

In order to analyze the behavior of the unit, a set of process variables was collected from the plant's distributed control system (DCS). The measurements correspond to three weeks of continuous operation in winter asset and three weeks in summer asset and the data are available as 3-minute averages. 27 process variables are available.

3.1 Analysis and inference

The operational objective of the column is to produce as much ethane as possible (minimizing concentration of propane from the top of the column) while satisfying the constraint on the amount of impurity from the bottom (maximum concentration of ethane in the bottom less than 2%). With respect to the loss of ethane from the bottom, such considerations led to the definition of 3 operational modes:

- A *normal* status, corresponding to the operation of the column, where the concentration of ethane is within allowable bounds (within 1.8 - 2.0%).
- A *high* status, corresponding to the operation of the column, where the concentration of ethane is exceeding the allowable upper bound (2%).
- A *low* status, corresponding to the operation of the column, where the concentration of ethane is below the allowable lower bound (1.8%)

The two abnormal conditions have a direct and important economic implication. In fact, when at *low* status, the process is delivering a product out of specifications, whereas when at *high* the product is within the specifications with unnecessary operational costs.

To understand under which conditions such modes are experienced, in a recent study (Corona, 2009) we analyzed the clustering structure of the process data and visualized the operating conditions of the unit. Starting from a selection of important process variables, we expanded this subset by incorporating an additional *dummy* indicator, specifically calculated to indicate the status. As such, the new variable was defined as to take values +1, -1 or 0, according to the operational status of the process. Value 0 is assigned to the *normal* operation, whereas values +1 and -1 correspond to *high* and *low* operations, respectively. Note that the calculation of the *dummy* variable required the availability of a real-time measurement for the ethane concentration: Such a variable is presently acquired from a continuous-flow chromatograph (GC). The subset of selected variables, augmented by the *dummy* indicator, was then used to calibrate a SOM over which the resulting component planes and U-matrix were analyzed. The exploration is a direct application of the techniques discussed in (Alhoniemi, 2002). The study allowed us to illustrate on simple displays how the clustering structure of the measurements corresponds to the operational modes of the deethanizer.

However, the delay associated with the analytical measurements of the ethane can pose severe limitations to the online analysis. Moreover, the existing instrumentation setup may benefit from a backup measurement for such an important variable. For such a reason, we are extending the analysis by validating its functionality when replacing the analytical measurements with online estimates. The availability of an inferential model would allow the development of an automated system to be implemented in the DCS.

For the purpose, a soft sensor based on a standard MLP with sigmoidal activation, was developed to infer the ethane concentration. The estimates are obtained starting from the same input subset of easily measurable process variables and selected according to the guidelines provided by Baratti et al. (1995). The MLP was optimized with the

Levenberg-Marquard method and cross-validation. In Fig. 2, the response of the sensor on a set of testing observations is reported for a week of continuous operation.

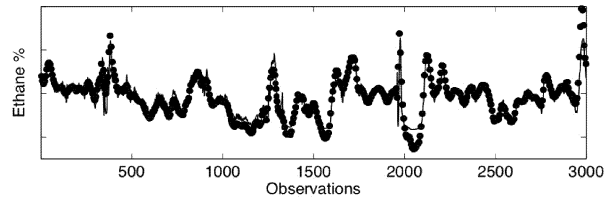


Figure 2 Ethane from the bottom: Analytical measurements (\bullet) and MLP estimates ($-$).

Based on the MLP estimates, a bi-dimensional SOM was calibrated using only the winter data. The map consists of a hexagonal array of prototype vectors initialized in the space spanned by the eigenvectors corresponding to the two largest eigenvalues of the covariance matrix of the data. As usual, the ratio between the two largest eigenvalues was used to calculate the ratio between the two dimensions of the SOM.

On the SOM, we analyzed the clustering structure of the data and visualized the operating conditions of the unit using the U-matrix and the component planes, Fig. 3.

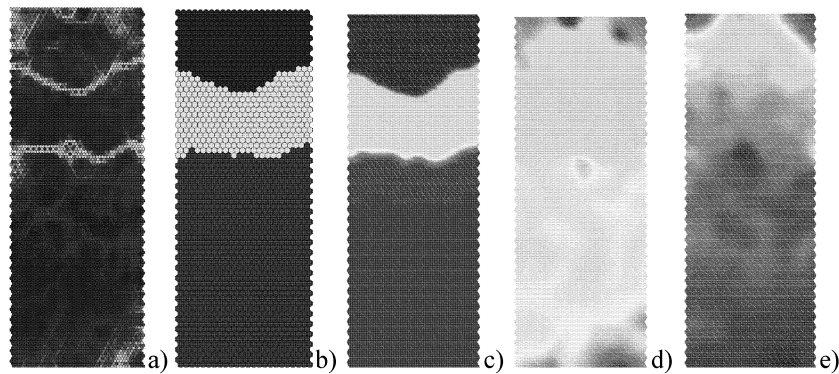


Figure 3 The U-Matrix (a), the SOM coloured according to the K-means algorithm (b), the component planes for the dummy variable (c), the estimated ethane concentration (d) and the temperature TI-1414 (e). The colouring scheme for the component planes (c, d, and e) differs from what defined for the K-means clustering (b).

The U-matrix is based on distances between each prototype vector and its immediate neighbors. A common way to visualize it consists of an initial projection of all the distances onto a color axis and the subsequent display with colored markers between each prototype vector. On the display, areas with homogeneous coloring correspond to small within-cluster distances, whereas cluster borders are areas with homogeneous coloring but corresponding to large between-cluster distances. In Fig. 3(a), distances are depicted with dark gray color shading toward light gray as the proximity between the prototypes decreases. The visualization permits to recognize the presence of three distinct clusters of prototypes, as well as several other data substructures. However, to

obtain a quantitative characterization of the clustering structure, the prototypes of the SOM should be regarded as a reduced data set and modeled with a standard clustering algorithm. For simplicity, we are here adopting a standard K-means algorithm coupled by the Davier-Bouldin index, a measure of cluster validity, to identify an optimal number of taxonomies from data (Milligan, 1985). As expected, optimality was found for three clusters, the operational modes of the deethanizer. On the SOM, such clusters are located in the lower, middle and upper part of the map. After coloring the SOM according to the cluster membership obtained by using the K-means algorithm, in Fig. 3(b), and comparing it with the component plane of the *dummy* variable, Fig. 3(c), it is straightforward to associate the three taxonomies to the three main operational modes.

Although apparently less evident, the same structuring is retrieved from the component planes of the estimated ethane concentration (in Fig. 3(d)) and one of the temperatures in the exhausting section of the deethanizer (in Fig. 3(e)). Looking for similar patterns in similar positions in such components planes allows the visualization of a neat dependence between the ethane composition and the temperature indicator. Such pair of variables shows near-identical but reversed component planes, thus highlighting the inherent inverse correlation that exists between them. Information about this dependence can be further enhanced by applying the coloring scheme resulting from clustering directly to the original observations in the time domain. Unfortunately, due to limitation in reporting colored figures, it is not possible appreciate this advantage.

So far, we have restricted the analysis only to the measurements observed under winter asset. However, it is also possible to directly use the calibrated SOM as a reference model for new and unseen observations: In our setting, the three weeks of data corresponding to the summer operation of the deethanizer column. To validate this idea, the winter SOM was used to explore the behavior of the deethanizer under summer asset. Again, the summer measurements from the GC were replaced by the estimates from the soft sensor. The analysis was accomplished by initially projecting the new data onto the calibrated SOM, being the mapping based on a nearest neighbor criterion between the new sample vectors and the prototype vectors of the SOM. Once the mapping is completed, the inspection the new data is performed on the calibrated SOM.

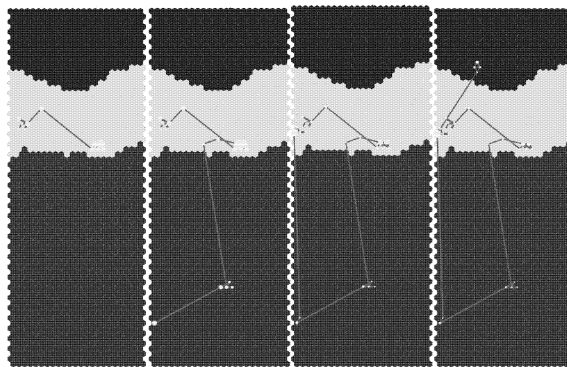


Figure 4 Trajectory of summer observations on the winter SOM (approx. 6hr).

The results in extrapolation are presented by illustrating another technique for visualization on the SOM. The approach allows to following the operational changes in the process and tries to provide a simple display for identifying reasons of specific behaviors. For the purpose, the map calibrated on the winter data can be enhanced by the inclusion of the summer point trajectories followed by the process. The trajectory, which passes through all the BMUs of each new data vector, is shown as segmented line connecting the visited prototypes, marked as by dots. The trajectory makes it possible to intuitively indicate the current mode of the process and observe how it has been reached. In the sequence of panels in Fig. 4, the process trajectory is reported for a small time window corresponding to six hours of continuous summer operation of the deethanizer. Following the temporal evolution, the diagrams show a process that is initially operated in *normal* condition. As the process moved further in time, new prototype vectors were visited and added to the trajectory until the column eventually leaves the normality region and crosses it towards the region of *high* ethane composition. In a similar fashion, all the process variables can be assigned a different coloring to match the visited modes. Such a representation would allow to appreciating that the change in the operation was mainly due to an abrupt change in feed flow-rate. Unfortunately, such a display cannot be reported because of the space limitation.

4. Conclusions

In this work, we implemented and discussed a strategy to model, visualize and analyze the information encoded in industrial process data using the Self-Organizing-Map. In particular, the proposed strategy was applied to an industrial distillation column allowing to individuating an alternative control strategy. Moreover, in order to overcome the problem associated with the time delay of the analytical instrumentation, a software sensor, based on a MLP neural network, was developed allowing the possibility to use such an approach also for an efficient online monitoring of the unit.

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