

NUTRIENTS AND CHEMICAL OXYGEN DEMAND (COD) REMOVALS BY MICROALGAE – BACTERIA CO-CULTURE SYSTEM IN PALM OIL MILL EFFLUENT (POME)

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ABSTRACT: In Malaysia, large amounts of waste known as palm oil mill effluent (POME) are generated during the production process of crude palm oil. Conventionally, POME is treated using biological treatment that involves two processes; aerobic and anaerobic. These processes however, require long hydraulic retention time and produce methane and carbon dioxide (CO₂) that can cause environmental problems. Alternatively, POME can be treated by a combination of microalgae and bacterial co-culture that requires a shorter treatment time and is environmentally friendly. In this study, a microalgae strain, *Chlorella vulgaris* was co-cultured with a bacteria strain *Azospirillum brasilense* in POME with an initial concentration of 1.9×10^6 cells/mL and 10^4 CFU/mL, respectively. The removal of chemical oxygen demand (COD) and nutrients (phosphorus and ammonium) were analyzed using Standard Methods, APHA 1999. The effectiveness of the co-culture system in POME treatment under agitation and aeration conditions for nutrients and COD removals were studied. Results show that the removal of ammonium by microalgae was much higher under the aeration condition (73.5%) compared to that of the agitation condition (34.4%) in POME. Moreover, co-culture system exhibits better removal of ammonium, phosphorus, and COD (84%, 87.3% and 51.8%, respectively) compared to that in an axenic microalgae system (67%, 84.2% and 41.1%, respectively). The kinetic studies on the co-culture system and the nutrients removal were also conducted. The kinetic coefficients of maximum specific growth rate (μ_{max}) and half-saturation coefficient (k_s) obtained from Lineweaver-Burk plot were 0.192 d^{-1} and 27.32 mg/L , respectively. Based on the findings obtained, the co-culture system could be implemented as an efficient and inexpensive alternative method for POME treatment.

ABSTRACT: Di Malaysia, banyak bahan buangan kilang minyak kelapa sawit yang dikenali sebagai (POME) telah terhasil ketika proses penghasilan minyak kelapa sawit mentah. Dahulu, POME dirawat menggunakan rawatan biologi yang terdiri daripada dua proses; erob dan anaerob. Walau bagaimanapun, proses-proses ini memerlukan masa yang panjang bagi pengekalan hidraulik dan gas metana dan karbon dioksida (CO₂) telah terhasil yang menyebabkan masalah alam. Sebagai alternatif, POME dapat dirawat dengan kombinasi mikroalga dan sistem bakteria ko-kultur melalui masa rawatan yang lebih pendek dan mesra alam. Kajian ini, strain mikroalga, *Chlorella vulgaris* telah di ko-kultur dengan strain bakteria *Azospirillum brasilense* dalam POME dengan ketumpatan awal 1.9×10^6 sel/mL dan 10^4 CFU/mL masing-masing. Penyingkiran kehendak oksigen secara kimia (COD) dan nutrisi (fosferus dan ammonium) telah dikaji menggunakan Kaedah Biasa, APHA 1999. Keberkesanan system ko-kultur dalam rawatan

POME di bawah keadaan kisaran dan pengudaraan bagi nutrisi dan penyingkiran COD telah diselidiki. Dapatan kajian menunjukkan penyingkiran ammonium menggunakan mikroalga lebih banyak melalui keadaan pengudaraan (73.5%) berbanding keadaan kisaran (34.4%) dalam POME. Tambahan, system ko-kultur menunjukkan lebih bagus dalam penyingkiran ammonium, fosferus dan COD (84%, 87.3% dan 51.8%, masing-masing) dibandingkan dengan sistem mikroalga aksenik (67%, 84.2% dan 41.1%, masing-masing). Kajian kinetik pada sistem ko-kultur dan penyingkiran nutrisi turut dijalankan. Pekali kinetik kadar maksimum pertumbuhan sebenar (μ_{max}) dan pekali separuh-penepuan (k_s) telah diperolehi melalui plot Lineweaver-Burk iaitu 0.192 d^{-1} dan 27.32 mg/L , masing-masing. Berdasarkan penemuan ini, sistem ko-kultur boleh dijalankan dengan cekap dan murah sebagai pilihan alternatif kepada rawatan POME.

KEYWORDS: *co-culture; microalgae; palm oil mill effluent; symbiotic; wastewater treatment*

1. INTRODUCTION

Malaysia is one of the largest producers and exporters of palm oil in the world. During the palm oil production process, huge amounts of wastewater, known as palm oil mill effluent (POME) consisting of various pollutants and nutrients, are generated [1]. POME contains a high concentration of phosphorus, organic nitrogen, and other nutrients. Moreover, the biochemical oxygen demand (BOD) and chemical oxygen demand (COD) content in POME are also high, reaching 100 times higher than municipal sewage [2]. Hence, POME treatment is very crucial prior to discharge into natural water resources, such as rivers, which can cause water pollution and negatively affect aquatic life.

POME has been treated using conventional methods (e.g. anaerobic and aerobic digestion). However, these methods produce CO_2 and methane which can lead to environmental problems. Furthermore, these conventional methods require long hydraulic retention time (HRT) and can take at least 20 days for the aerobic digestion process. As an alternative for POME treatment, utilization of microalgae has been introduced due to its ability to grow in robust environments and still remove various pollutants in wastewater such as phosphorus and nitrogen. It was also reported that bacteria known as microalgae growth promoting bacteria (MGPB) can be co-cultured with microalgae to improve the removal of nutrients [3-6]. Moreover, this co-culture system shares a symbiotic relationship. The oxygen (O_2) produced by microalgae during photosynthesis will be used by heterotrophic bacteria and the bacteria in return release CO_2 that can be consumed by microalgae for growth [7].

The aim of this study is to evaluate the efficiency of microalgae and bacteria species, *Chlorella vulgaris* and *Azospirillum brasilense* for nutrients (ammonium and phosphorus) and COD removals in partially treated POME under different cultivation conditions to replace the aerobic digestion process in the conventional POME treatment. The kinetics studies of the co-culture system were also determined.

2. METHODOLOGY

2.1 Raw Materials and Inoculum Preparation

A species of microalgae (*Chlorella vulgaris*) and a bacteria strain (*Azospirillum brasilense*) were used in this study. The microalgal strain and bacteria were purchased from Universiti Malaya, Kuala Lumpur and Leibniz-Institute DSMZ, Germany respectively. Microalgae was grown in Tris-Acetate-Phosphate (TAP) medium at 25°C and 150 rpm in a rotary shaker and bacteria was maintained in nutrient media at $30\pm 2^\circ\text{C}$ and 120 rpm [3]. Partially treated palm oil mill effluent (POME) (sample after anaerobic process) was

collected from West Mill Sdn Bhd, Sime Darby Research Centre, Carey Island, Malaysia. Partially treated POME was used because this study aims to replace the aerobic process and the amount of nutrients available were acceptable for microalgae to growth. Sample obtained was stored in 5 L plastic containers and kept at 4 °C to limit the activity of biodegradation process and prevent any contamination [7]. The ammonium, phosphorus and COD contents in partially treated POME are 162, 18, and 874 mg/L, respectively.

2.2 Experimental Set Up

Microalgae and bacteria were cultivated in POME at 10% concentration ($V_{\text{microalgae} - \text{bacteria}} / V_{\text{POME}}$) in a 250 mL flask for 6 days and 25 ± 2 °C under $45 - 50 \mu\text{mol photon m}^{-2}\text{s}^{-1}$ of illumination of white fluorescent light (alternate 12 h/12 h of light/dark periods) [7]. The initial concentrations of microalgae and bacteria were 1.9×10^6 cells/mL and 10^4 CFU/mL respectively [7].

Two different cultivation conditions of microalgae – bacteria for POME treatment, agitation and aeration conditions, were tested. For the agitation condition, POME treatment was incubated in incubator shaker at 25 °C and 150 rpm. For the aeration condition, a shake flask containing POME and microbes was connected to an air pump (1.8 L/min) to provide aeration to the treatment system. A sterilized 0.22 μm nylon filter was used to avoid contamination. During cultivation, 2 mL of algae suspension was collected for every 2 days and filtered using 0.45 μm nylon filter before it was analyzed for ammonium, phosphorus and COD using their respective method. The growth of microalgae and bacteria were also recorded.

2.3 Analytical Methods

Microalgae cell number was calculated by Neubauer haemocytometer counting and bacterial concentrations were determined as colony forming units (CFU) on nutrient media agar plates. Besides that, the Standard Methods for the Examination of Water and Wastewater were used to analyse ammonium, phosphorus and COD removal [8]. Ammonium content was analysed using phenate method while phosphorus content (orthophosphate) was analysed using ascorbic acid method and COD was analysed using closed reflux, colorimetric method [7].

2.4 Kinetics Study

Based on the best growth conditions (agitation or aeration) in terms of COD and nutrient removal, batch kinetics studies were carried out by using approximately 1.9×10^6 cells/mL and 10^4 CFU/mL of microalgae and bacteria initial concentration, respectively. They were cultivated in partially treated POME at room temperature (25 ± 2 °C). POME was diluted to study the kinetics of different N/P ratios. The removals and the growth of microalgae were recorded and analyzed for six days of treatment. Kinetics coefficient, maximum specific growth rate, μ_{max} (d^{-1}) and half-saturation coefficient, k_s (mg/L) were determined using Lineweaver–Burk plot of $1/\mu$ vs. $1/S$.

3. RESULTS AND DISCUSSION

3.1 POME Treatment in Agitation and Aeration Conditions

The characteristic of the partially treated POME sample collected is tabulated in Table 1.

Table 1: Characteristic of partially treated POME

Parameters	Concentration (mg/L), except for pH and turbidity	Average Concentration (mg/L)
pH	7.5 – 8.5	8
COD	600 – 900	750
Ammonium	160 – 250	205
Phosphorus	10 – 30	20
Total Suspended Solid	1120 – 1160	1140
Total Volatile Solid	880 – 1170	1025
Turbidity (NTU)	2755 – 2785	2775
Oil and Grease Content	118 - 234	176

In this study, microalgae were grown in non-sterilized partially treated POME under agitation and aeration cultivation conditions. Throughout the treatment, the pH of POME was observed and measured. At day 0, the pH of POME samples was 7.5 and it increased to 8.8 after six days of treatment in both conditions. The percentage of ammonium, phosphorus, and COD removal by agitation and aeration conditions in non-autoclaved partially treated POME are illustrated in Fig. 1.

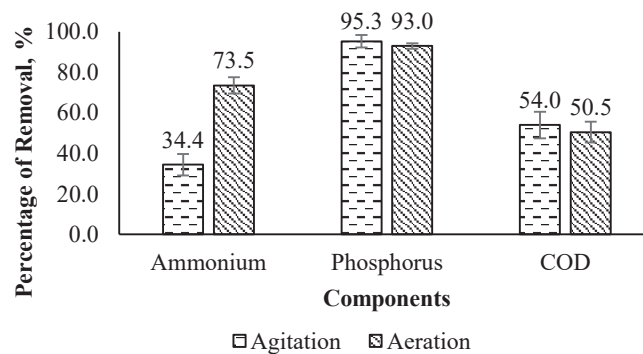


Fig. 1: Percentage of ammonium, phosphorus, and COD removal in agitation and aeration conditions by axenic microalgae in a 250 mL flask containing 150 mL non-sterilized partially treated POME with 10% concentration ($V_{\text{microalgae} - \text{bacteria}} / V_{\text{POME}}$) for 6 days at 25 ± 2 °C and under $45 - 50 \mu\text{mol photon m}^{-2}\text{s}^{-1}$ of illumination of white fluorescent light (alternate 12 h/12 h periods of light/dark). Initial concentration of Ammonium = 162 mg/L, Phosphorus = 18 mg/L and COD = 874 mg/L. Error bars represent one standard deviation about the mean ($n = 3$).

Based on Fig. 1, the removal of ammonium in aeration condition is 73.5% which is higher compared to that in agitation condition which is 34.4%. The ammonium removal percentage was in line with the growth rate of *C. vulgaris* which were 0.356 d^{-1} and 0.176 d^{-1} for aeration and agitation system respectively. Similar results were obtained whereby the microalgae cultivated with air supply (aerated) recorded higher growth rate compared to the microalgae grown in mixing shaker (non-aerated system) [9]. The optimum turbulence effect created by aeration system promotes better cell growth which consequently helps in the removal of the nutrients. Moreover, under equal light intensity, air flux is produced as a result of the turbulence and creates different movement regimes of the cells within the media. Adequate turbulence enhances mass transfer of nutrients to the microalgae cell and

promotes gas exchange that overcomes the photo-oxidative effect as well as minimizing thick boundary layer between microalgae cell and the surrounding condition of unstirred suspension. In addition to that, sufficient system turbulence enhances the microalgae reproduction compared to the non-aerated medium, which can cause biomass accumulation [9].

Although the removals of phosphorus and COD in the agitation system were higher compared to those in the aeration system, the difference was very small, i.e. less than 5%. Results indicated that the aeration system offered better nutrient removal especially for ammonium removal. Therefore, the aeration system was chosen to be used in the subsequent experiment.

3.2 Axenic and Co-culture Systems in Aeration Condition

A co-culture system (*C. vulgaris* and *A. brasilense*) was utilized in the partially treated POME treatment. In this case, sterilized partially treated POME was used with initial concentration of 874 mg/L, 162 mg/L and 18 mg/L of COD ammonium and phosphorus, respectively. The microalgae – bacteria growth conditions were at 0.77 g/L (1.9×10^6 cells/mL), 10^4 CFU/mL and day 1.52 for microalgae initial concentration, bacteria initial concentration and bacteria inoculation time, respectively. POME treatment was conducted in the aeration condition. The growth profiles of microalgae – bacteria and percentage of nutrients and COD removals in axenic and microalgae – bacteria co-culture systems are shown in Fig. 2 (a) and 2 (b), respectively.

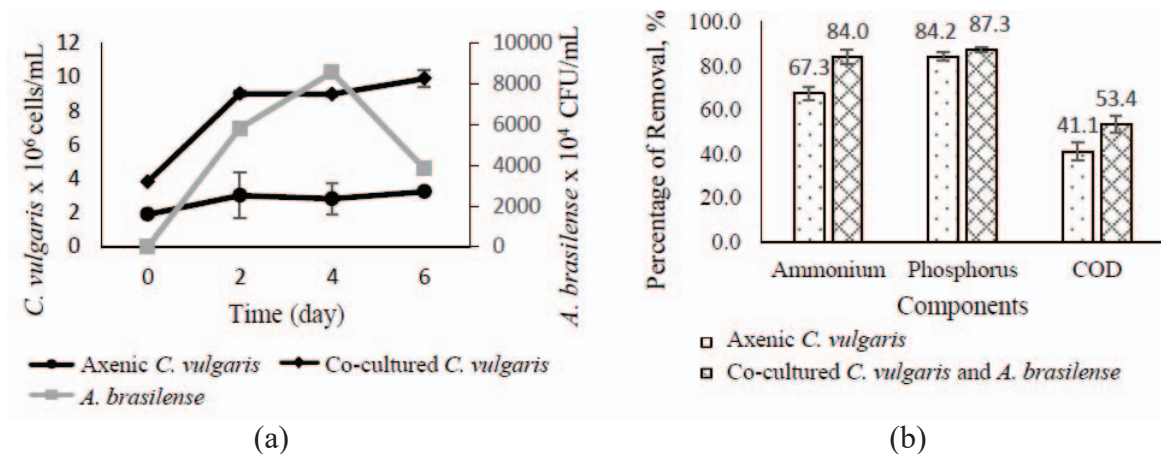


Fig. 2: (a) Growth profiles of bacteria (*A. brasilense*), microalgae (*C. vulgaris*) in axenic system and microalgae (*C. vulgaris* and *A. brasilense*) in co-culture system (b) Percentage of ammonium, phosphorus and COD removals in aeration condition by axenic microalgae and co-culture microalgae – bacteria in a 250 ml flask containing 150 mL sterilized partially treated POME with 10% concentration ($V_{\text{microalgae} - \text{bacteria}}/V_{\text{POME}}$) for 6 days at 25 ± 2 °C, under $45 - 50 \mu\text{mol photon m}^{-2}\text{s}^{-1}$ of illumination of white fluorescent light (alternate 12 h/12 h periods of light/dark) and aerated. Initial concentration of Ammonium = 162 mg/L, Phosphorus = 18 mg/L and COD = 874 mg/L. Error bars represent one standard deviation about the mean ($n = 3$).

Figure 2 (a) shows that, co-culture of microalgae and bacteria enhanced the microalgae population. The specific growth rate of co-cultured microalgae was higher (0.570 d^{-1}), compared to that of axenic microalgae (0.228 d^{-1}). Similar results were obtained by a study that reported that the growth of *C. vulgaris* was significantly enhanced when co-

immobilized with *A. brasilense* bacteria under aeration conditions (1.8 L/min) [3]. It was also reported that some bacteria species enhance microalgae cells growth [10]. However microalgae and bacteria have a complex relationship. It depends on the species of microalgae and bacteria as well as the growth conditions themselves [5,11]. Mutual symbiosis between microalgae and bacteria can be achieved if the species and conditions were optimum for both microorganisms. The results showed that bacteria promoted the growth of microalgae when the initial concentration was suitable (10^4 CFU/mL) and cultivated under aeration conditions. A study reported that, at low bacteria concentration (10^2 CFU/mL), the effect of bacteria in the co-culture system was not significant towards the removal of the nutrients. On the other hand, low nutrient removal was also recorded at maximum bacteria concentration (10^6 CFU/mL) due to the competition of the nutrients between the bacteria and microalgae. At these conditions, the bacteria growth rate was higher than the microalgae growth rate, hence the utilization of nutrients was dominated by the bacteria cells [7].

In addition, *A. brasilense* bacterium was able to grow well with microalgae and partially treated POME with specific growth rates of 2.264 d^{-1} . Besides getting oxygen from the microalgae's photosynthesis process, the aeration process helps to promote gaseous exchange and enhances mass transfer of nutrients in the system. Moreover, excess oxygen from microalgae photosynthesis can be released from the media in the aeration system [10].

Based on Fig. 2 (b), the co-culture system has significantly increased the removals of COD and nutrients after six days of treatment, especially for ammonium and COD removal. The presence of bacteria delivers positive effect to the system. Higher percentage removals of ammonium, phosphorus and COD were obtained for co-cultured *C. vulgaris* system (84%, 87.3% and 53.4%, respectively) compared to that from axenic *C. vulgaris* system (67.3%, 84.2%, and 41.1%, respectively). These results show better removals of COD and nutrients compared to another study that reported that microalgae from *Chlamydomonas incerta* species removed 67.35% of COD with initial concentration of 250 mg/L in POME in 28 days [1]. Ammonium removal in this study was slightly lower (84%) compared to the previous study, which used *Spirulina plantesis* to achieve 96.5% removal from approximately 296 mg/L of initial concentration [2]. Comparison of DOE standard and results of removals achieved by this study is presented in Table 2.

Table 2: DOE standard B and final results of removals achieved by this study

	DOE Standard B	This Study		
		Initial Concentration		Final Concentration
		Axenic and Co- cultured System	Axenic System	Co-cultured System
COD (mg/L)	200	874	514.8 ± 37.32	407.3 ± 32.95
Ammonium (mg/L)	20	162	53 ± 4.97	25.9 ± 5.3
Phosphorus (mg/L)	10*	18	2.84 ± 0.39	2.29 ± 0.15

* DOE Standard B for sewage discharge into enclosed water body

Results obtained in this study showed that, microalgae – bacteria co-cultured system exhibits a good potential to be applied in POME treatment within six days of cultivation compared to aerobic digestion process that required at least 20 days of treatment with final concentration 200, 52 and 12 mg/L of COD, nitrogen and phosphorus respectively [1]. The co-cultured system also proves that, it enhances the COD and nutrient removal in the

treatment compared to the axenic system. However, further investigation has to be conducted to improve COD removal in order to achieve the standard set by DOE, Malaysia, prior to discharge treated POME into the river. Heterotrophic bacteria is one of the microorganisms that have an important role in the reduction of COD content by breaking down the organic matter in the wastewater. Isolation and growth characterization of heterotrophic bacteria in partially treated POME sample could be investigated further in order to find more efficient bacteria to improve COD removals in POME.

3.3 Kinetics Studies of Microalgae Growth and Nutrients Removal

There are two important nutrients for microalgae growth: phosphorus (P) and ammonium (N). Kinetics constants were determined to study the rate of nutrients uptake by the microalgae. In this study, nutrients removal rates were calculated by Eq. (1) [12].

$$R = \frac{C_0 - C_t}{t_t - t_0} \quad (1)$$

where R represents the removal rate of nutrients (N or P), C_0 and C_t represent initial concentration of nutrients and nutrient concentration at time t_t respectively and t_t is the time when there is no significant change of nutrient concentration. The specific nutrient removal rate, R_t was determined by dividing R by the initial cell density (*C. vulgaris*). In these kinetic studies, two POME samples with different N/P ratio were utilized. The N/P ratio of media used for POME 1 and POME 2 were 8.96 and 2.27 respectively. The specific nutrient removal rate, R_t of ammonium and phosphorus for both samples are shown in Table 3.

Table 3: Specific nutrient removal rate of ammonium and phosphorus in POME 1 and POME 2

Samples	N/P Ratio	R_N (mg g ⁻¹ d ⁻¹)	R_P (mg g ⁻¹ d ⁻¹)
POME 1	8.96	29.42	3.41
POME 2	2.27	4.64	1.18

The specific ammonium removal rates, R_N for *C. vulgaris* grown in POME 1 and POME 2 were 29.42 and 4.64 mg g⁻¹d⁻¹ with initial ammonium concentration (POME 1 = 167 mg/L, POME 2 = 22.6 mg/L). These results showed that high R_N was achieved when initial concentration of ammonium introduced was high. These results were in agreement with a previous study whereby the specific N removal rates of *Chlorella* sp. grown in media with 9 and 56 N/P were 1.8 and 3.8 mg mg⁻¹ Chl a d⁻¹ respectively [12]. Furthermore, the other study observed that the specific N removal rates increased from 0.5 to 3 mg mg⁻¹ Chl a d⁻¹ when the initial concentration of NH₄⁺-N increased from 13.2 mg/L to 410 mg/L in synthetic wastewater [12].

In this study, a similar pattern of results was obtained for specific phosphorus removal rates, R_P . The R_P increased from 1.18 to 3.41 mg g⁻¹d⁻¹ with the increase of phosphorus initial concentration from 9.96 to 18.06 mg/L. Slightly higher P concentration in the primary effluent also led to higher R_P . *Chlorella* sp. obtained 0.25 and 0.15 mg mg⁻¹ Chl a d⁻¹ for the diluted sludge centrate and the primary effluent with initial P, 4.0 and 3.5 mg/L respectively [12].

First-order and second-order reactions were tested for both nutrients removal to find the reaction constant. The reaction constant for first-order and second-order was calculated by Eq (2) and (3), respectively [13].

$$-\ln \frac{C_N}{C_{NO}} = kt \quad (2)$$

$$-\ln \frac{C_P C_{NO}}{C_N C_{PO}} = (C_{PO} - C_{NO})kt \quad (3)$$

where C_N or C_P and C_{NO} or C_{PO} represent the concentration of ammonium or phosphorus at time t and t_0 , respectively and k is the reaction constant. Graphs were plotted for both order reactions and in this study, the removal of phosphorus and ammonium fitted most to the first-order reaction since R^2 in first-order reaction for both POME were higher than R^2 in second-order reaction, as shown in Table 4. This result was in line with a study that reported that the phosphorus and nitrogen removal in their study fitted the first-order reaction very well [12]. Based on the nutrient consumption, the yield of biomass was determined by Eq. (4), [11].

$$Y = \frac{X_i - X_0}{C_0 - C_i} \quad (4)$$

where Y represents the yield of biomass linked to the consumption of nutrients (phosphorus, P or ammonium, N), C_0 is the initial nutrient concentration, C_i is the concentration of nutrients when there was no significant decrease of nutrients, X_i represents *C. vulgaris* cell density with respect to the nutrient C_i and X_0 is the initial *C. vulgaris* cell density [11]. The yield of biomass based on specific nutrient consumption and first order reaction rate constants are shown in Table 5.

Table 4: Value of R^2 for first and second order reaction

Sample	First-Order		Second-Order
	R^2, P	R^2, N	R^2, NP
POME 1	0.9305	0.9565	0.9231
POME 2	0.8741	0.9127	0.8052

Table 5: Kinetics parameters of nutrients removal for *C. vulgaris* in POME 1 and POME 2

Sample	k_P	k_N	Y_N	Y_P	Y_P/Y_N
POME 1	0.3685	0.3272	0.01406	0.1213	8.6231
POME 2	0.1271	0.1383	0.1751	0.6886	3.9327

The biomass yield based on N consumption, Y_N , for *C. vulgaris* cultivated in POME 1 was lower than the yield in POME 2 which were 0.01406 g mg⁻¹ N and 0.1751 g mg⁻¹ N respectively. A similar result was obtained for Y_P , 0.1213 g mg⁻¹ P and 0.6886 g mg⁻¹ P for *C. vulgaris* grown in POME 1 and POME 2, respectively. The ratio of Y_P/Y_N , indicates the amount of the ratio of N/P required (mg N consumed/mg P consumed) to produce the same unit amount of biomass. In this study, N/P ratio of POME 1 was almost double the N/P ratio of POME 2. Theoretically, the chemical formula of microalgae is C₁₀₆ H₁₈₁ O₄₅ N₁₆ P where N/P ratio is 7.2 [14]. The Y_P/Y_N for *C. vulgaris* cultivated in POME 1 was 8.62, which is close to this theoretical value.

In this study, the final N and P concentration in POME 1 were 25.9 and 2.3 mg/L respectively. This case was similar to the result obtained by a study that stated that P was the limiting nutrient for microalgae grown in POME 1. Thus, the kinetic coefficients of

microalgae growing in POME 1 were determined using Lineweaver-Burk equation (Eq. (5)), where μ is specific growth rate (d^{-1}), μ_{max} is the maximum specific growth rate (d^{-1}), S is the concentration of limiting nutrient (mg/L) and k_s is half-saturation coefficient (mg/L). Experimental data were plotted as illustrated in Fig. 3 [11].

$$\frac{1}{\mu} = \frac{k_s}{\mu_{max}} \frac{1}{S} + \frac{1}{\mu_{max}} \quad (5)$$

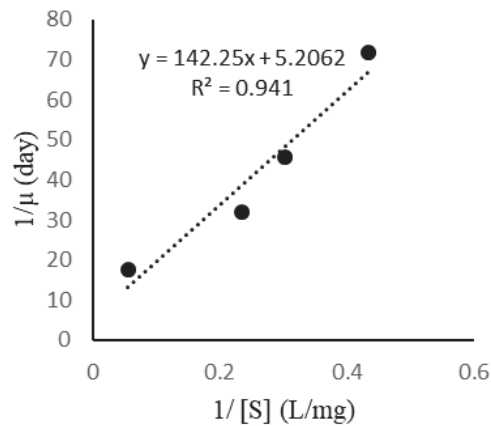


Fig. 3: Lineweaver-Burk plot used to estimate kinetic coefficient.

Based on the linear fit line for this plot (Fig. 3), the kinetic coefficients μ_{max} and k_s of P removal by *C. vulgaris* were determined to be $\mu_{max} = 0.192 d^{-1}$ and $k_s = 27.32 mg/L$ ($R^2 = 0.973$).

4. CONCLUSION

As a conclusion, higher removal of ammonium from POME was obtained under aeration conditions (73.5%) compared to that of agitation conditions (34.4%). In addition, the microalgae – bacteria co-culture system showed higher removal of ammonium, phosphorus, and COD in POME (84%, 87.3% and 51.8%, respectively) compared to that in the axenic microalgae system (67%, 84.2% and 41.1%, respectively). The kinetic coefficients obtained were $\mu_{max} = 0.192d^{-1}$ and $k_s = 27.32 mg/L$. The obtained data showed that this co-culture system has the potential to improve the current aerobic digestion process in the wastewater treatment. The long HRT required by the aerobic treatment can be shortened by replacing or integrating with this co-culture system. Moreover, this system also promotes green technology and can be considered for future commercial use. However, for COD removal, further investigation on POME treatment is required in order to achieve the standard set by DOE, Malaysia, prior to discharge into the river.

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