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MHD STAGNATION POINT FLOW WITH THERMAL RADIATION AND SLIP EFFECT OVER A LINEAR STRETCHING SHEET

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ABSTRACT

This research investigates the flow of stagnation point magnetohydrodynamic (MHD) and heat transfer along the stretched sheet in the existence of radiation and slip effects. With the help of similarity variables, the governing partial differential equations (PDEs) are transformed into ordinary differential equations (ODEs). The BVP4C technique in Matlab function has been used to simplify the governing ODEs. The numerical outcomes for temperature and velocity profiles, coefficient of skin friction and Nusselt Number have been achieved and matched with the findings in literature. The findings are compared to previously reported results. In addition, the impacts of numerous related parameters on the profiles of velocity and temperature are shown, and the results of every related parameter are presented using graphs. The velocity profile decreases as the magnetic force, suction, and permeability parameters rise.

Keywords: Thermal radiation; slip effect; magnetohydrodynamic (MHD); suction; Prandtl number

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1. INTRODUCTION

In scientific literature, an extensive body of research has been done using stagnation points over the stretching sheet. It is widely used in a variety of engineering and manufacturing area, including insulating materials, polymer sheet production, glass drawing, production, displacement, and continuous casting, it is well-known in the researchers. With the use of comparable variables, Hiemenz [1] claimed that equations of Navier–Stokes may be translated into 3rd order ODEs, which became known as two-dimensional stagnation point flow. Sakiadis [2] gave mathematical solutions for boundary layer flow on the stretched surface in his paper. The exponentially stretched surface and the linearly stretched surface were further developed by Crane [3] in 1970. Chiam [4] investigated the flow of a stagnation point towards a bending plate. Several researchers, including Ishak et al. [5], have studied the MHD flow of stagnation point approaching a vertical stretched surface. Sadeghy et al. [6] examined flow of stagnation point of Maxwell fluid in a twodimensional. Attia [7] studied the viscous fluid flow affecting on a porous stretched sheet for heat absorption in three dimensions using hydromagnetic flow of laminar and stagnation point. Recently, Ghasemi and Hatami [8] explored the stagnation point of nanofluid flow in conjunction with the effects of solar radiation for MHD nanofluid flow.

As a result of recent advances in research, magnetohydrodynamics (MHD) may be thought of the mix of mechanics of fluids and electromagnetism, specifically the action of magnetic on an electrically conducting fluid, or both. Many studies have recently concentrated on the study of MHD flow because of its importance in a wide range in the field of Plasma Physics and engineering applications, including oil refinery, MHD power generators, the reactor of nuclear power, chemical reactions, magnetic mixers, and boundary layer control in aerodynamics [9-12]. Here, we will discuss several recent research that has concentrated on the MHD influence on heat transfer and flow concerns. These studies also focused on the flow and heat transfer of a viscous and incompressible fluid passing through a stretching surface along with magnetic field, among other fluids that are used in the industrial setting. According to Darzi et al. [13], for instance, they looked at the impact of heat transfer via the porous medium on the profile of velocity and temperature due to a thin liquid film flowing through a stretching sheet.

Nandeppanavar et al. [14] used a porous stretched sheet and thermal radiation to investigate the MHD flow of stagnation point 2D via a porous medium. Abel and Nandeppanavar [15] investigated the impacts of non-uniform temperature sources and thermal radiation on MHD viscoelastic fluid movement and heat transmission past a stretched surface. Mustafa and Khan [16] explored the 2D steady next to the boundary, the mass transfer of Casson nano fluid, and the heat transmission of this liquid in existence of an exponential stretched surface. Khalili et al. [17] quantitatively examined heat transfer of MHD flow of three distinct nanofluids induced through the shrunk plane inside porosity medium. Ghasemi et al. [18] simulated the MHD blood flow through porous vessels using both analytical and numerical methods. They classified blood like a 3rd grade fluid comprising nanoparticles, according to their classification. Asadi et al. [19] study the natural CuO-TiO2/water hybrid nanofluid at two infinite parallel vertical plates that are infinitely parallel to one another. They discovered that as volume percentage of nanoscale particles improves, width of momentum boundary increases while width of thermal layer decreases.

Several practical applications relating to the boundary flow immerse in media of porous, including heat exchangers, geothermal engineering, oil industries, nuclear waste destruction, system of the grain storage, and others have drawn great interest to the research of boundary layer flow embedded in porous medium. Nield and Bejan [20] have highlighted the advantages of heat transfer flow across porous material and how it might be used. Several researchers, including Mohanty et al. [21], have studied approximate solutions for the transport of heat and mass of a micropolar fluid passing through porous media. Working on the MHD convective flow with reaction of chemical and radiation on porous medium [22]. Prasad et al. [23] explored the oscillatory reaction on viscoelastic fluid passing in porous media caused by a stretched sheet in a porous media. A study by Shamshuddin et al [24] investigated flow of MHD of the micropolar liquid using permeable medium over a moving surface that was incline. Many of the authors have recently completed simulations of porous medium interactions under a variety of flow conditions, which are detailed in the references [25-30].

This study expands the prior model of Agbaje et al. [31] to include the impact of MHD slip and radiation on heat transfer owing to flow of stagnation of nano-liquid across the stretching surface, which was previously neglected. Because of the linear similarity conversions, the conservation equalities are reduced to a dimensionless state. In order to simulate the nanofluid, an condition interfacial boundary is introduced, and an effective and reliable numerical approach, the BVP4C technique in Matlab function, according to the authors. Detailed research is conducted to determine how important parameters affect flow rate and energy output. The findings have been supported by results from prior investigations, which have been tabulated and found to have an excellent connection with the findings of the current study.

2. PROBLEM FORMULATION

In this study considered steady, MHD fluid flow in a porous form of boundary layer towards the stagnation point with effect of slip and thermal radiation long a stretched surface. The free stream velocity $U_{\infty}(x) = bx$ and the stretching velocity $U_w(x) = ax$ are along the flow direction. The constants a and b areas a > 0 and $b \ge 0$. The ambient temperature is T_{∞} and the mass flux velocity is $V_w(x)$. The flux velocity $V_w(x) = -(av)^{1/2}S$. The surface temperature of the stretching sheet is $T_w(x) = T_{\infty} + cx^n$, where c and n are constant as c > 0 at the heated surface. The proposed model is demonstrated using the following set of PDEs [31]. The physical model is presented in Figure 1.



Figure 1. Geometry of Fluid Flow Model.

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \qquad (1)$$

$$u\frac{\partial u}{\partial x} + v\frac{\partial v}{\partial y} = U_{\infty}\frac{dU_{\infty}}{dx} + v\frac{\partial^2 u}{\partial y^2} + \sigma\frac{B_0^2}{\rho}(U_{\infty} - u)$$

$$+ \frac{v}{K}(U_{\infty} - u), \qquad (2)$$

$$u\frac{\partial T}{\partial x} + v\frac{\partial T}{\partial y} = \alpha\frac{\partial^2 T}{\partial y^2} + \frac{Q}{\rho c_p}(T - T_{\infty}) - \frac{\alpha}{K}\frac{\partial q_r}{\partial y}, \quad (3)$$

with the boundary conditions

 $u = U_w(x) + L\left(\frac{\partial u}{\partial y}\right), v = V_w(x), T = T_w(x), \text{when } y = 0$ $u \to U_\infty(x), T \to T_\infty \text{asy} \to \infty$ (4) In the system of equations (1)-(4) u, v are the velocity components along the axis of x, y respectively. The parameters are $\rho, v, K, \alpha, c_p, Q, L, \sigma$ and q_r the fluid density, kinematic viscosity, porous medium permeability, thermal diffusivity, specific heat capacity, heat source/sink (Q > 0, Q < 0), slip effect, electrical conductivity, and heat flux.

PDEs (2-3) are transformed into ODEs using similarity transformation.

$$f(\eta) = \frac{\psi}{(a\nu)^{\frac{1}{2}x}}, \theta(\eta) = \frac{T - T_{\infty}}{T_w - T_{\infty}}, \eta = (\frac{a}{\nu})^{\frac{1}{2}y}, \quad (5)$$

 ψ is the stream function and its definition is as follows:

$$u = \frac{\partial \psi}{\partial y} and \ v = -\frac{\partial \psi}{\partial x} \tag{6}$$

The velocity components u and v became.

$$u = axf'(\eta), v = -(av)^{\frac{1}{2}}f(\eta)$$
 (7)
Where (') represents differentiation w.r.t. η ,
 γ is the suction/injection parameter where
 $\gamma > 0$ shows suction effect and $\gamma < 0$
indicates the injection effect. The
transformed ODEs are as

$$\begin{aligned} f''' + ff'' - f'^2 + B^2 + M(B - f') - (\Gamma - B)f', \quad (8) \\ \frac{1}{P_r} \left(1 + \frac{4}{3}R\right)\theta'' + A\theta + f\theta' - n\theta f' \end{aligned}$$

The boundary conditions are as

$$f(0) = \gamma, f'(0) = 1 + \delta f''(0), \theta(0) = 1,$$

$$f'(\infty) = B, \theta(\infty) = 0$$
(10)

Where $B = \frac{b}{a}$ is velocity ratio, $M = \frac{\sigma B_0^2}{a\rho}$ is magnetic, $\Gamma = \frac{v}{aK}$ is the permeability

parameter, $A = \frac{Q}{a\rho c_p}$ is the dimensionless heat generation/absorption coefficient, $R = \frac{4\sigma^*T_{\infty}^3}{KK_s}$ is the thermal radiation and $\delta = (\frac{b}{\gamma})^{1/2}L$ is the slip parameter.

The "substantial physical quantities of interest are the skin friction C_f and Nusselt number Nu_x are as

$$\begin{split} \mathcal{C}_{f} &= \frac{\tau_{w}}{\rho_{f} U_{\infty}^{2}}, N u_{x} \\ &= \frac{x q_{w}}{K_{f} (T_{w} - T_{\infty})}, \end{split} \tag{11} \\ \text{where } \tau_{w} \quad \text{is the shear stress along the} \\ \text{plate's surface and } q_{w} \text{ is the heat flow from} \\ \text{the plate, the equations are as follows:} \end{split}$$

$$\tau_{w} = \mu \left(\frac{\partial u}{\partial y}\right)_{y=0}, q_{w}$$

= $-K \left(\frac{\partial T}{\partial y}\right)_{y=0} + (q_{r})_{y=0},$ (12)

Putting Equation (5) into Equation (11) with (10), one can get

$$C_f Re_x^{\frac{1}{2}} = f''(0), \frac{Nu_x}{Re_x^{\frac{1}{2}}}$$
$$= -\left(1 + \frac{4}{3}R\right)\theta'(0), \qquad (13)$$
Where $Re_x = \frac{U_w(x)x}{x}$ is the Reynolds number.

3. NUMERICAL PROCEDURE AND VALIDATION

We used the Three Stage Labatto Three A Scheme in conjunction with the BVP4C technique to numerically solve the transformed ODEs (08-10) in order to find the solution. To make the problem simpler, all of the modified equations are expressed in the form of an initial value problem (IVP). In this case the initial values of f''(0) and $\theta'(0)$ are not known. The BVP4C is used to determine the of f''(0) and $\theta'(0)$ by picking a specific value of $\eta \rightarrow \infty$ and a few starting guesses. The procedure of forecasting initial guesses is repeated until the desired value of the iteration is achieved. To turn Equations (08-10) into the first order ODEs, we must take into account the following variables:

$$f = y_1, f' = y_2, f'' = y_3, \theta = y_4, \theta' = y_5$$
(14)

$$f''' = y_2 * y_2 - y_1 * y_3 - B^2 - M * (B - y_2)$$
(15)

$$\theta'' = \left(\frac{3 * Pr}{3 + 4 * R}\right) \{n * y_4 * y_2 - A * y_4 - y_1$$
(16)

Subject to boundary conditions

 $y_1(0) = \gamma, y_2(0) = 1 + \delta * \alpha_1, y_3(0) = \alpha_1$ $y_4(0) = 1, y_5(0) = \alpha_2$ (17)

where α_1 and α_2 are assumed initial guesses which need to be determined. When $M = \gamma = A = R = \delta = 0$ and Pr = 0.7, comparisons of coefficient of skin friction for various rates of *B* with earlier published findings [31-33] are stated in Table 1 to assess the validity of the current numerical results. Also found is that an excellent link between the two variables has been established. Moreover, it is noted that a high degree of correlation is obtained.

Table 1. Values of f''(0) for some values of *B* at $M = \gamma = A = R = \delta = 0$ and Pr = 0.7.

В	[31]	[32]	[33]	Present results
0.01	-0.9980	-0.9980	-0.99802	-0.998065
0.02	-0.9958	-	-0.99578	-0.995811
0.05	-0.9876	-	-0.98757	-0.987588
0.10	-0.9694	-0.9694	-0.96938	-0.969387
0.20	-0.9181	-0.9181	-0.91810	-0.918107
0.50	-0.6673	-0.6673	-0.66732	-0.667263
1.00	-	-	0.00000	0
2.00	-	2.0175	2.01750	2.0175027
3.00	-	4.7292	4.72928	4.729282
4.00	-	-	-	8.000429

4. **RESULTS AND DISCUSSIONS**

This section illustrates and discusses the effects of various relevant parameters such as velocity ratio parameter *B*, magnetic parameter M, permeability parameter Γ , heat generation/absorption coefficient A_{i} thermal radiation R, Prandtl number Pr, and slip effect δ graphically on velocity and temperature profiles. In Figures 2-11, extensive numerical solutions are presented. The default values of the parameters considered as under, unless mentioned: $\gamma = 1, \Gamma = 0.1, \delta =$ otherwise 0.1, n = 0.2, A = B = M = 0.1, and Pr = 0.7. In Tables 2 and 3, coefficient of skin friction and heat transfer rate for different thermal radiation and velocity slip parameter values are listed. The effects of radiation Rparameter on the temperature and velocity profiles are illustrated in Figures 2-3, respectively. A rise in the radiation parameter results cause to rise in the temperature of the fluid being heated. Essentially, the radiative energy enhances the impact of temperature and conduction at respective place on the surface, as a result, a vast amount of radiation energy is created, which raises the temperature of the fluid. On the other hand, there is no noticeable change in the profile of velocity as a horizontal surface has been considered.

Table 2. Results of f''(0) and $-\theta'(0)$ for different values of *R* with $\gamma = 1, \Gamma = 0.1, \delta = 0.1, n = 0.2, A = B = M = 0.1$ and Pr = 0.7.

R	<i>f</i> ″′(0)	$-oldsymbol{ heta}'(oldsymbol{0})$
0	-1.338191965	0.945955902
0.3	-1.338191965	0.705378882
0.6	-1.338191965	0.574614931

Table 3. Results of f''(0) and $-\theta'(0)$ for different values of δ when = 1, Γ = 0.1, n = 0.2, A = B = M = 0.1 and Pr = 0.7.

δ	<i>f</i> ″(0)	$-oldsymbol{ heta}'(0)$
0	-1.616258037	0.729409419
0.1	-1.338191965	0.705378882
0.3	-1.006890697	0.673515832



Figure 2. Temperature profile at different values of R with $\gamma = 1, \Gamma = 0.1, \delta = 0.1, n = 0.2, A = B = M = 0.1$



Figure 3. Velocity profile at different values of R with $\gamma = 1, \Gamma = 0.1, \delta = 0.1, n = 0.2, A = B = M = 0.1$ and Pr = 0.7.

Figures 4-5 illustrate the influence of the velocity slip parameter δ on the profiles of temperature and velocity in the presence of the other parameters. When slip effects grow, it has been observed that the

temperature increases. However, by gradually increasing the values of the velocity slip parameter, it is possible to achieve a steady reduction in the velocity profiles. The effect of the "Prandtl number Pr on the temperature profile is depicted and seen in the Figure 6. The Prandtl number is defined as the ratio of the momentum diffusivity to the thermal diffusivity of a given system. The increase in the values of Pr leads in a decrease in the temperature profile, which in turn results in a decrease in the thickness of the thermal boundary layer. definitely, a lesser thermal diffusivity causes a rise in the Prandtl number, which in turn aids in the reduction of the thickness of the thermal boundary layer. Because of this increase in the Pr, the flow at the boundary is pulled down, resulting in a change in the thickness of the thermal boundary layer.



Figure 4. Temperature profile at different values of δ with $\gamma = 1$, $\Gamma = 0.1$, n = 0.2, R = 0.3, A = B = M = 0.1 and Pr = 0.7.



Figure 5. Velocity profile at different values of δ with $\gamma = 1$, $\Gamma = 0.1$, n = 0.2, R = 0.3, A = B = M = 0.1and Pr = 0.7.



Figure 6. Temperature profile at different Pr with $\gamma = 1, \Gamma = 0.1, n = 0.2, A = 0.1, R = 0.3, B = 0.1$ and M = 0.1.

The effects of the suction parameter γ on the fluid velocity and temperature profiles are illuminated in Figures 7-8, respectively. From this point on, we can see that the profile reduces with an increase in the value of γ . The corresponding boundary layer thickness is also reduced, owing to the fact that the suction produces a reduction in the flow of the stream in a vertically descended manner. Also shown in Figure 8 is the relationship between the temperature and the suction/injection parameter γ . It is obvious that increasing γ decreases the temperature field. Because applying suction causes the number of fluid particles to be drawn into the wall, the temperature boundary layer drops.



Figure 7. Velocity profile at different values of γ with $\Gamma = 0.1, n = 0.2, R = 0.3, A = B = M = 0.1$ and Pr = 0.7.



Figure 8. Temperature profile at different values of γ with $\Gamma = 0.1, n = 0.2, R = 0.3, A = B = M = 0.1$ and Pr = 0.7.

The values of $-\theta'(0)$ in the solution for the variation of *Pr* are shown in Figure 9, and it come to be positive for greater Prandtl number, indicating that heat moves from the heated surface to the ambient temperature of fluid. This fact also lends

support to the previous findings of the current study, which show that temperature falls as the Prandtl number rises in significance. Furthermore, when the radiation parameter is expanded, the rate heat transfer reduces; of this fact demonstrates that heat flows from the ambient temperature in the direction of the surface. Slip heated effects, notwithstanding this, have the influence of slowing down the rate of heat transmission, as seen in Figure 10. The results of Figure 11 similarly corroborate those of Figure 10, where the heat transfer rate decreases as the thermal radiation parameter is raised to greater levels.



Figure 9. Temperature variation at different values of *Pr* with *R* at $\gamma = 1, \Gamma = 0.1, n = 0.2, A = 0.1, B = 0.1$ and M = 0.1.



Figure 10. Temperature variation at different values of δ with *R* at $\gamma = 1$, $\Gamma = 0.1$, n = 0.2, A = 0.1, B = 0.1, M = 0.1 and Pr=0.7.



Figure 11.Temperature variation at different values of R with δ at $\gamma = 1$, $\Gamma = 0.1$, n = 0.2, A = 0.1, B = 0.1, M = 0.1 and Pr = 0.7

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onceptualization, Ubaidullah Yashkun & Khairy Zaimi; Methodology, Ubaidullah Yashkun & Liaquat Ali Lund; Software, Ubaidullah Yashkun; Formal analysis, Ubaidullah Yashkun, Khairy Zaimi, Liaquat Ali Lund; Writing—original draft, Ubaidullah Yashkun & Liaquat Ali Lund; Supervision, Khairy Zaimi. All authors have read and agreed to the published version of the manuscript.

CONCLUSION

The aim of the current study was to offer a Three Stage Labatto Three a formula for addressing boundary value problems that included physical effects of various parameters. The equations of the electrically conducting incompressible fluid flow moving towards stagnation point through the stretched surface are approximated numerically in this study, and

the results are presented in this paper. Flow modelling in porous media considers the impacts of heat source and sink, thermal radiation, velocity slip, magnetic field, and suction/injection parameters. Nonlinear ODEs are obtained from PDEs by the simulations of appropriate similarity transformations. Using the Three Stage Labatto Three A formula, the approximate solutions generated for the parameters: Nusselt number, skin friction coefficient, temperature profile, and velocity profile. The accuracy of the used method is validated by comparing current results to published literature. previously The following are the effects of relevant parameters:

- a. When the suction parameter was set to greater levels, the conductivity of the skin friction increased.
- b. The increasing value of the radiation parameter has ensured that the temperature profile along with the thickness of the thermal boundary layer have both raised.
- c. The amount of suction *S* introduced into a steady fluid flow reduces the fluid flow velocity and temperature.
- d. The increasing Prandtl number has guaranteed that profile of temperature and the thickness of the thermal layer have both decreased.
- e. Because of a rise in the permeability parameter, the thickness of the boundary layer is increased.

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